AMENDMENTS TO THE CLAIMS

- 1. (Original) A heterogeneous ruthenium catalyst comprising silicon dioxide as support material, wherein the catalyst surface comprises alkaline earth metal ions (M^{2^+}) and the alkaline earth metal ions (M^{2^+}) are introduced into the catalyst surface by impregnating a preliminary heterogeneous ruthenium catalyst with a solution of an alkaline earth metal(II) salt.
- 2. (Original) The ruthenium catalyst according to claim 1, wherein the catalyst surface comprises magnesium ions (Mg²⁺).
- 3. (Currently amended) The ruthenium catalyst according to claim 1 or 2, wherein the catalyst comprises from 0.1 to 10% by weight of ruthenium and the catalyst surface comprises from 0.01 to 1% by weight of the alkaline earth metal ion(s) (M²⁺), in each case based on the weight of the silicon dioxide support material.
- 4. (Currently amended) The ruthenium catalyst according to claim 1 or 2, wherein the catalyst comprises from 0.2 to 5% by weight of ruthenium and the catalyst surface comprises from 0.05 to 0.5% by weight of the alkaline earth metal ion(s) (M²⁺), in each case based on the weight of the silicon dioxide support material.
- 5. (Currently amended) The ruthenium catalyst according to any of the preceding elaims claim 1, wherein the catalyst is produced by single or multiple impregnation of the support material with a solution of a ruthenium(III) salt, drying and reduction.
- 6. (Currently amended) The ruthenium catalyst according to the preceding claim claim 1, wherein the solution of an alkaline earth metal(II) salt is an aqueous solution of magnesium nitrate or calcium nitrate.
- 7. (Currently amended) The ruthenium catalyst according to any of the preceding elaims claim 1, wherein the support material based on amorphous silicon dioxide has a BET surface area (in accordance with DIN 66131) in the range from 30 to 700 m²/g.

8. (Currently amended) The ruthenium catalyst according to any of the preceding elaims claim 1, wherein the catalyst comprises less than 0.05% by weight of halide (<u>as</u> determined by ion chromatography), based on the total weight of the catalyst.

- 9. (Currently amended) The ruthenium catalyst according to any of the preceding elaims claim 1, wherein the ruthenium is concentrated as a shell at the catalyst surface.
- 10. (Currently amended) The ruthenium catalyst according to the preceding claim 9, wherein the ruthenium in the shell is partially or fully crystalline.
- 11. (Currently amended) The ruthenium catalyst according to any of the preceding claims claim 1, wherein the alkaline earth metal ion(s) is/are ions are highly dispersed in the catalyst surface.
- 12. (Currently amended) The heterogeneous ruthenium catalyst according to any of the preceding claims claim 1, wherein the percentage ratio of the signal intensities of the Q_2 and Q_3 structures Q_2/Q_3 in the silicon dioxide support material determined by means of solid-state ²⁹Si-NMR is less than 25.
- 13. (Currently amended) The ruthenium catalyst according to any of the preceding claims claim 1, wherein the total concentration of Al(III) and Fe(II and/or III) in the silicon dioxide support material is less than 300 ppm by weight.
- 14. (Currently amended) A process for hydrogenating a carbocyclic aromatic group to form the corresponding carbocyclic aliphatic group, wherein a comprising contacting the carbocyclic aromatic group with a heterogeneous ruthenium catalyst, according to any of claims 1 to 13 is used wherein the catalyst comprises silicon dioxide as support material, and the catalyst surface comprises alkaline earth metal ions (M²⁺) and the alkaline earth metal ions (M²⁺) are introduced into the catalyst surface by impregnating a preliminary heterogeneous ruthenium catalyst with a solution of an alkaline earth metal (II) salt.

15. (Currently amended) The process according to the preceding claim for hydrogenating claim 14, wherein the carbocyclic aromatic group is a benzene ring to form the corresponding carbocyclic 6-membered ring.

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16. (Currently amended) The process as claimed in either of the two preceding elaims claim 15 for preparing a bisglycidyl ether of the formula I

where R is CH₃ or H, by ring hydrogenation of the corresponding aromatic bisglycidyl ether of the formula II

- 17. (Currently amended) The process according to claim 16, wherein the aromatic bisglycidyl ether of the formula II which is used has a content of corresponding oligomeric bisglycidyl ethers of less than 10% by weight.
- 18. (Currently amended) The process according to claim 16, wherein the aromatic bisglycidyl ether of the formula II which is used has a content of corresponding oligomeric bisglycidyl ethers of less than 5% by weight.
- 19. (Currently amended) The process according to either of the two preceding claims claim 18, wherein the oligomeric bisglycidyl ethers have a molecular weight in the range from 568 to 1338 g/mol for R = H and a molecular weight in the range from 624 to 1478 g/mol for $R = CH_3$.

20. (Currently amended) The process according to any of claims 14 to 19 claim 14, wherein the hydrogenation is carried out conducted at a temperature in the range from 30 to 200°C.

- 21. (Currently amended) The process according to any of claims 14 to 20 claim 14, wherein the hydrogenation is earried out conducted at absolute hydrogen pressures in the range from 10 to 325 bar.
- 22. (Currently amended) The process according to any of claims 14 to 21 claim 14, wherein the hydrogenation is earried out conducted over a fixed bed of catalyst.
- 23. (Currently amended) The process according to any of claims 14 to 21 claim 14, wherein the hydrogenation is carried out conducted in a liquid phase in which the catalyst is comprised in the form of a suspension.
- 24. (Currently amended) The process according to any of claims 16 to 23 claim 16, wherein the aromatic bisglycidyl ether of the formula II is used as a solution in an organic solvent which is inert toward the hydrogenation with the solution comprising from 0.1 to 10% by weight, based on the solvent, of water.
- 25. (Currently amended) The process according to any of claims 14 to 24 claim 14, wherein a the solution of the substrate aromatic bisglycidyl ether of the formula II to be hydrogenated which comprises alkali earth metal ions (M²⁺) is used.
- 26. (Currently amended) The process according to any of claims 14 to 24 claim 14, wherein a the solution of the substrate aromatic bisglycidyl ether of the formula II to be hydrogenated which comprises magnesium ions (Mg²⁺) is used.
- 27. (Currently amended) The process according to either of the two preceding claims claim 25, wherein the alkaline earth metal ion content of the solution is from 1 to 100 ppm by weight.
- 28. (Currently amended) The process according to claim 25 or 26, wherein the alkaline earth metal ion content of the solution is from 2 to 10 ppm by weight.

29. (Currently amended) The process according to any of claims 14 to 28 claim 27 for preparing a bisglycidyl ether of the formula I.

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where R is CH₃ or H, which have a content of corresponding oligomeric ring-hydrogenated bisglycidyl ethers of the formula

where n = 1, 2, 3 or 4, of less than 10% by weight.

- 30. (Currently amended) The process according to the preceding claim 29, wherein the bisglycidyl ether of the formula I has a content of corresponding oligomeric ring-hydrogenated bisglycidyl ethers of less than 5% by weight.
- 31. (Original) The process according to claim 29, wherein the bisglycidyl ether of the formula I has a content of corresponding oligomeric ring-hydrogenated bisglycidyl ethers of less than 1.5% by weight.
- 32. (Original) The process according to claim 29, wherein the bisglycidyl ether of the formula I has a content of corresponding oligomeric ring-hydrogenated bisglycidyl ethers of less than 0.5% by weight.

33. (Currently amended) The process according to any of claims 29 to 32 claim 29, wherein the content of oligomeric ring-hydrogenated bisglycidyl ethers is determined by heating the aromatic bisglycidyl ether for 2 hours at 200°C and for a further 2 hours at 300°C, in each case at 3 mbar.

- 34. (Currently amended) The process according to any of claims 29 to 32 claim 29, wherein the content of oligomeric ring-hydrogenated bisglycidyl ethers is determined by GPC measurement (gel permeation chromatography[[])] (GPC).
- 35. (Currently amended) The process according to the preceding claim 34, wherein the content of oligomeric bisglycidyl ethers in % by area determined by GPC measurement is equated to a content in % by weight.
- 36. (Currently amended) The process according to any of claims 29 to 35 claim 29, wherein the bisglycidyl ether of the formula I has a total chlorine content determined in accordance with DIN 51408 of less than 1000 ppm by weight.
- 37. (Currently amended) The process according to any of claims 29 to 36 claim 29, wherein the bisglycidyl ether of the formula I has a ruthenium content determined by mass spectrometry in combination with inductively coupled plasma (ICP-MS) of less than 0.3 ppm by weight.
- 38. (Currently amended) The process according to any of claims 29 to 37 claim 29, wherein the bisglycidyl ether of the formula I has a platinum-cobalt color number (APHA color number) determined in accordance with DIN ISO 6271 of less than 30.
- 39. (Currently amended) The process according to any of claims 29 to 38 claim 29, wherein the bisglycidyl ether of the formula I has an epoxy equivalent weight determined in accordance with the standard ASTM-D-1652-88 in the range from 170 to 240 g/equivalent.
- 40. (Currently amended) The process according to any of claims 29 to 39 claim 29, wherein the bisglycidyl ether of the formula I has a proportion of hydrolyzable chlorine determined in accordance with DIN 53188 of less than 500 ppm by weight.

41. (Currently amended) The process according to any of claims 29 to 40 claim 29, wherein the bisglycidyl ether of the formula I has a kinematic viscosity determined in accordance with DIN 51562 of less than 800 mm²/s at 25°C.

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- 42. (Currently amended) The process according to any of claims 29 to 41 claim 29, wherein the bisglycidyl ether of the formula I has a cis-cis:cis-trans:trans-trans isomer ratio in the range 44-63%:34-53%:3-22 %.
- 43. (Currently amended) The process according to any of claims 29 to claim 42, wherein the bisglycidyl ether is obtained by complete hydrogenation of the aromatic rings of a bisglycidyl ether of the formula II

where R is CH₃ or H, with the degree of hydrogenation being > 98%.